

*Article*

## Effect of the Molten Metal Stream's Shape on Particle Size Distribution of Water Atomized Metal Powder

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**Abstract.** The current knowledge indicated that water pressure, molten metal temperature, water flow rate and water jet configuration are very important factors which affect on the particle size distribution and shapes of atomized powder. This study aimed to investigate whether the shape of molten affects the particle size of atomized powder. The experiments were the production of copper powder with the fixed atomization process conditions, but varied the shape of molten metal by using two different shapes of tundish nozzle's orifice to make the round and rectangular cross section of molten metal stream. There were three sizes for each orifice shape to determine the rate of production (metal flow rate) at 13 kg/min, 19 kg/min and 26 kg/min. The results showed that at the same flow rate of molten metal the production of flat metal stream from rectangular orifice made higher yield of finer particle, smaller median size (D50) and narrower range of size distribution than the production with the round cross section orifice for every production rates.

**Keywords:** Metal powder, water atomization, particle size distribution, tundish.

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## 1. Introduction

The metal powder used in the manufacturing process must have appropriate properties such as size, shape, and size distribution. Particle size is one of the most important properties to be considered, for using finer resolution powder enhances the accuracy of the work piece [1].

Atomization is one of the leading forerunners among the most promising and economic techniques for the fabrication of powders. the commonly applied mechanism for atomization involves the disintegration of liquid into a fine spray of droplets by high-velocity fluids [2].

Powder production, using an atomization process, has been being widely investigated and applied in industry [3], due to its advantages including high capacity, high flexibility for both elemental and pre-alloyed powder production and capability for rapidly solidified metal powder production. The rapidly solidified metal powders usually exhibit superior properties caused by fine microstructure, chemical homogeneity, extended solid solution and metastable phase formation. Therefore, metal parts produced from the rapidly solidified metal powders show superior mechanical properties.

In principle, when the metal melt is caused unstable by any forces it will be broken into forms of smaller pieces or droplets. Melt disintegration mechanism is shown in Fig.1 [4].

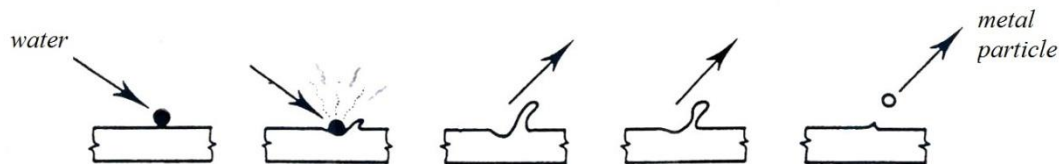


Fig. 1. The schematic steps involved in the “scrape” mechanism of water atomization [4].

Atomization begins with melting of metal. The liquid metal flows through a sized orifice from a tundish nozzle. Liquid flow is impinged by a high velocity stream of water. This breaks the liquid stream into particles that solidify rapidly. Particle size and shape are greatly influenced by the atomizing medium, pressure, and flow rate [5, 6].

For commercial practice of production of copper powder, liquid copper is superheated to about 1,150 to 1,200 °C, utilizing flow rates of 27 kg/min or more. Generally, to produce -100 mesh (-149 micron) copper powder, water pressure of 10 to 14 MPa (1,500 to 2,000 psi) is used. Atomization may be conducted in an air or inert (nitrogen) environment [7]. The typical yield of producing -325 mesh (-44 micron) powder with atomization method is from 25 to 80 percent [8].

High Pressure water atomization can provide fine powder. With increasing atomization water pressure, the particle size tends to become finer and particle size distribution also tends to become broader [9].

German (2001) reported the result of steel powder producing using 1.7 MPa water pressure and the obtained average particle size is 117  $\mu\text{m}$  stating that if the water pressure is increased to 13.8 MPa, the average particle size decreases to 42  $\mu\text{m}$  [10].

Seki et al. (1990) found that to produce finer particle resolution of 10  $\mu\text{m}$ , the process must operate with higher water pressure called High-Pressure Water Atomization (HPWA) which required very high water pressure up to 70 MPa. They also presented the relationship between the average metal particle diameter and the atomization pressure for two types of water atomization process as the following equations [11]:

$$D = 68P^{0.56} \text{ for V-jet water nozzle} \quad (1)$$

$$D = 114P^{0.58} \text{ for cone water nozzle} \quad (2)$$

where D is average metal particle size ( $\mu\text{m}$ ) and P is water pressure (MPa). The above equations were based on the result of the atomization of Fe-Ni alloy, carbon steel, high-speed tool steel, and pure nickel. It also shows that higher pressure water was needed to produce finer resolution powder.

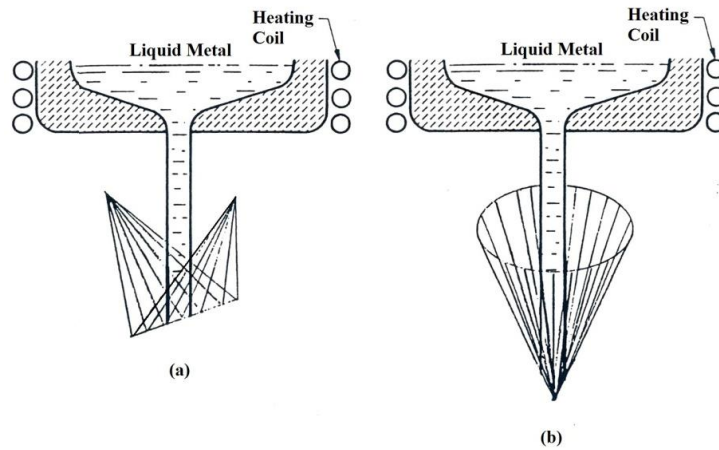


Fig. 2. Type of water jet in water atomization process (a) V-jet and (b) cone jet [10].

Grandzol (1973) showed a simple relationship between the average particle size,  $D$  ( $\mu\text{m}$ ), and the water velocity,  $V_w$  (m/s), which later modified by Grandzol and Tallmadge [12] to yield.

$$D = S / (V_w \sin \alpha) \quad (3)$$

where  $\alpha$  is the angle between the water jet axis and the molten metal stream axis and  $S$  is the normal velocity component.

In the previous studies, Yenwiset S. and Yenwiset, T. (2010) reported that using double V-jet water atomization made resolution metal powder finer than using cone water nozzle at the same water pressure [13] and in 2011 reported that higher water pressure and higher metal's superheat temperature made more yield of finer particles [14].

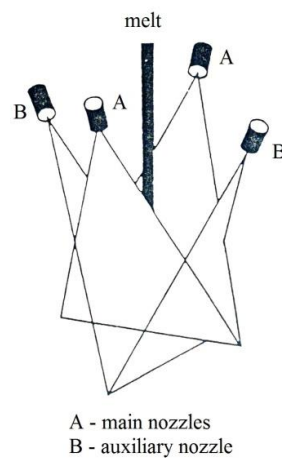


Fig. 3. Schematic of double V-jet water atomization [15].

M. Pasupathy et al. (2011) studied about the effect of the atomizer geometrical configuration on particle size and shape of atomized powder and the results showed that when impact angle is increased and/or water jet length reduced, the obtained powder becomes finer and more irregular [16].

From the information above, it is clear that to produce very fine metal powder, the process requires much energy for very high water pressure and very high superheat temperature of metal. However, besides the above variables, the shape of the molten metal stream may affect the production of metal powders as well.

The experiment was set by producing copper powder using the different tundish nozzle's shape and size while the other process condition were same. The objective of this study is to find out whether the shape of molten metal stream can affect the particle size and size distribution.

## 2. Experimental

### 2.1. Material

Material employed for this study was copper with 99% purity.

### 2.2. Variable

Two shape of tundish nozzle's orifice were used in the experiments to make round sectional metal stream and flat rectangular sectional metal stream.

To emphasize at the effect of metal stream shape, the metal flow rate from the two different shapes of nozzle orifice are controlled to nearly equal by using the similar size of cross-sectional area to avoid the effect of different metal flow rate.

However, three different sizes for each shape were applied to the experiment to validate whether the metal stream shape affecting on the particle size of powder.

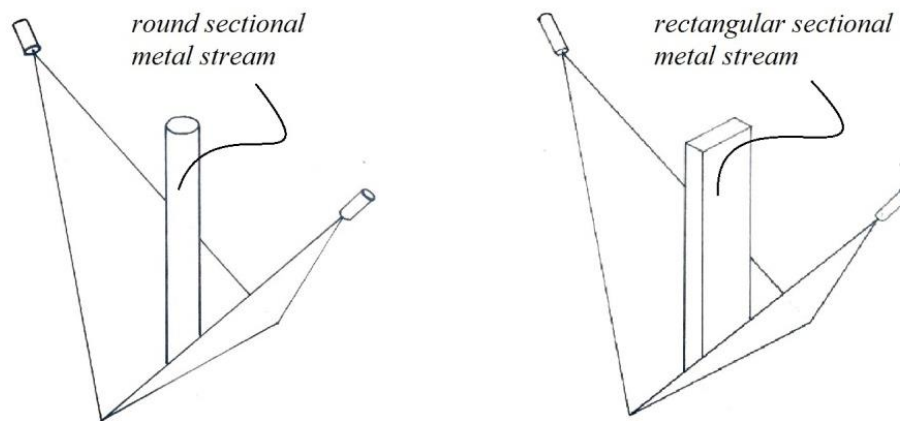


Fig. 4. Metal streams from round sectional orifice and rectangular sectional orifice.

Table 1. Tundish nozzle orifice's shapes and sizes used in the experiment.

Round sectional orifice			Rectangular sectional orifice			Approximate metal flow rate
call sign	diameter	cross sectional area	call sign	dimension	cross sectional area	
A1	5 mm	19.63 mm <sup>2</sup>	B1	3 mm * 6.5 mm	19.5 mm <sup>2</sup>	~ 13 kg/min
A2	6 mm	28.27 mm <sup>2</sup>	B2	3 mm * 9.5 mm	28.5 mm <sup>2</sup>	~ 19 kg/min
A3	7 mm	38.48 mm <sup>2</sup>	B3	3 mm * 12 mm	39.0 mm <sup>2</sup>	~ 26 kg/min

### 2.3. Operating Conditions in Water Atomization

The water atomization process used double V-jet nozzle (see Fig. 3) with the conditions and machine configurations as shown in Table 2 and Fig. 5. The fixed values are chosen because they are the best condition for the machine which provided the highest yield of fine particle from the previous studies [13, 14].

Table 2. Water atomization process conditions.

Parameter	Value
Metal superheated temperature	150 °C
Water Pressure (before nozzle)	11 MPa
Water Flow Rate (per each nozzle)	20 L/min
Total Water Flow Rate (all 4 nozzles)	80 L/min
Spread Fan Angle of Water Jet	20 °
Width of Water Intersection (w)	100 mm
Main V-Jet Angle ( $\gamma$ )	80 °
Auxiliary V-Jet Angle	70 °
Metal Stream Falling Distance (h)	300 mm

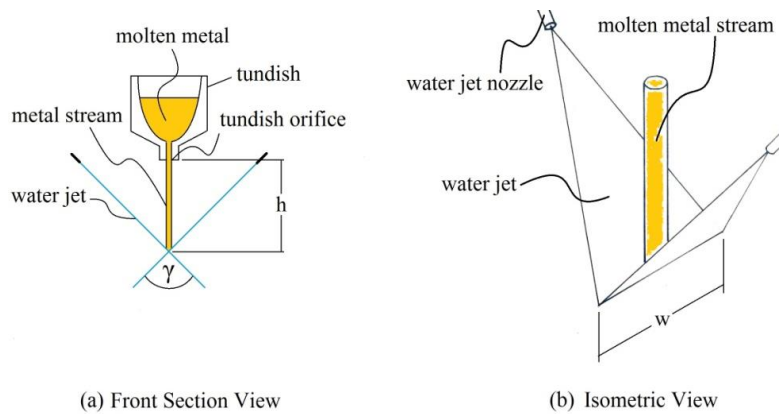


Fig. 5. Water atomization machine's configuration: (a) front sectional view and (b) isometric view.

#### 2.4. Experimental Procedure

From Table 1, six different tundish orifices were applied into the experiment. Three replicates were produce with each orifice and 15 kilogram of copper was produced for each batch. Therefore, a total 45 kilogram of copper was produced for each orifice.

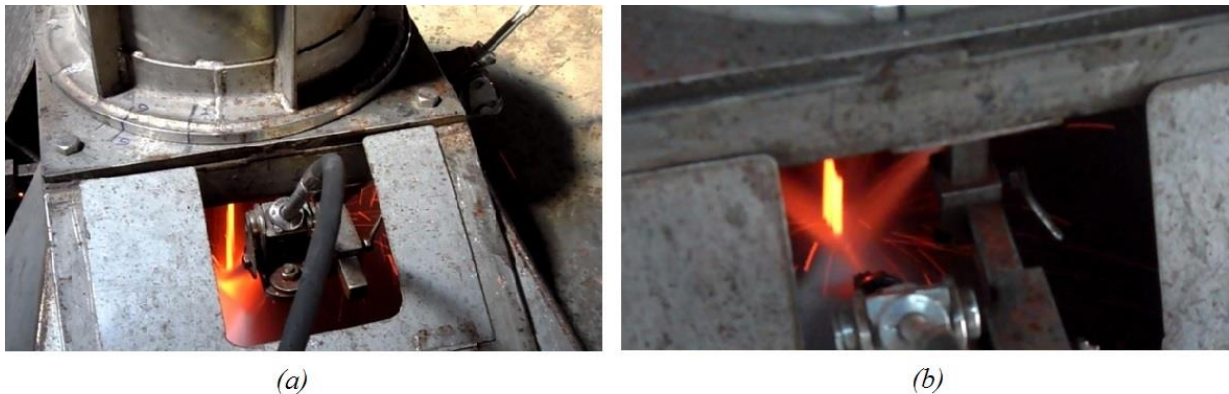


Fig. 6. Water atomization process: (a) using round orifice; and (b) using rectangular orifice.

### 3. Results and Discussions

Sieve analysis using the standard wire cloth sieves (ASTM E11) is the most widely used method of determining particle size distribution of metal powder [17]. The copper powder produced from each orifices were taken to investigate their particle size distribution by sieving. The sieve analysis results (average from 3 replicates) are shown from Table 3 to Table 5. The S-curves created from the result are shown from Fig. 7 to Fig. 9

Table 3. Sieved size distribution of copper powder produced at 13 kg/min metal flow rate.

ASTM-E11 Sieve Designation No.	Standard Size ( $\mu\text{m}$ )	Produced with A1 ( $\varnothing 5$ mm orifice)		Produced with B1 (3 mm x 6.5 mm orifice)	
		%	%	%	%
		Retained	Cumulative Passing	Retained	Cumulative Passing
100	150	6.8	93.2	4.7	95.3
120	125	0.9	92.3	1.1	94.2
140	106	3.6	88.7	2.6	91.6
170	90	4.1	84.6	5.2	86.4
200	75	9.3	75.3	6.8	79.6
230	63	8.4	66.9	9.2	70.4
270	53	13.1	53.8	11.8	58.6
325	45	12.6	41.2	13.4	45.2
400	38	16.7	24.5	16.1	29.1
450	32	13.3	11.2	15.3	13.8
500	25	7.0	4.2	8.5	5.3
pan	0	4.2	-	5.3	-

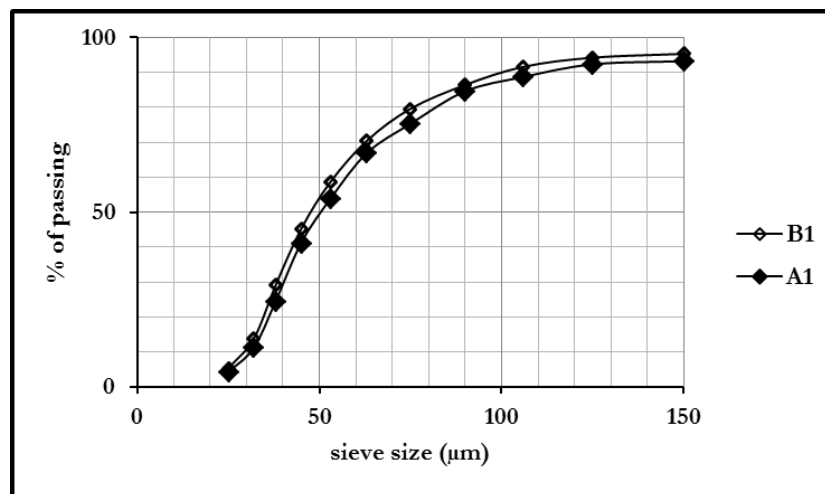
Fig. 7. Cumulative percentage of undersize of copper powder produced with metal flow rate  $\sim 13$  kg/min.

Table 4. Sieved size distribution of copper powder produced at 19 kg/min metal flow rate.

ASTM-E11 Sieve Designation No.	Standard Size ( $\mu\text{m}$ )	Produced with A2 ( $\varnothing 6$ mm orifice)		Produced with B2 (3 mm x 9.5 mm orifice)	
		%	%	%	%
		Retained	Cumulative Passing	Retained	Cumulative Passing
100	150	8.6	91.4	6.9	93.1
120	125	3.4	88.0	1.9	91.2
140	106	5.9	82.1	3.6	87.6
170	90	6.8	75.3	5.2	82.4
200	75	7.5	67.8	9.3	73.1
230	63	9.5	58.3	9.6	63.5
270	53	15.7	42.6	13.9	49.6
325	45	16.9	25.7	15.3	34.3
400	38	9.4	16.3	14.1	20.2
450	32	8.7	7.6	10.8	9.4
500	25	4.8	2.8	6.2	3.2
pan	0	2.8	-	3.2	-

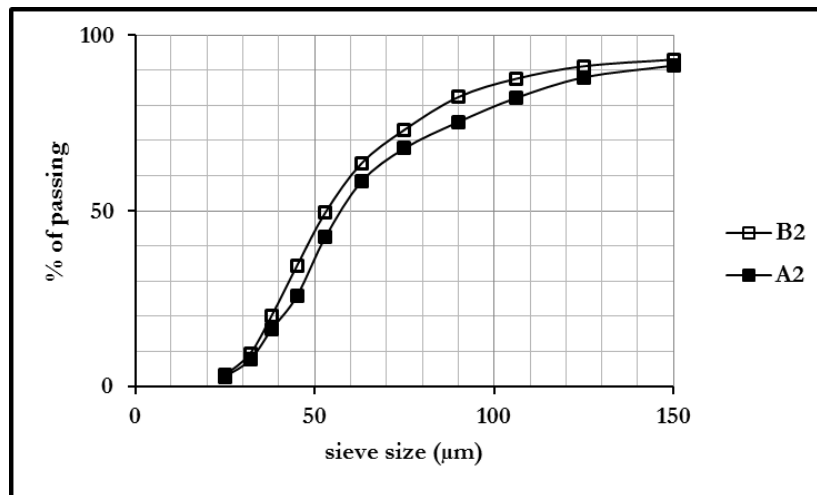


Fig. 8. Cumulative percentage of undersize of copper powder produced with metal flow rate ~ 19 kg/min.

Table 5. Sieved size distribution of copper powder produced at 26 kg/min metal flow rate.

ASTM-E11 Sieve Designation No.	Standard Size (µm)	Produced with A3 (Ø6 mm orifice)		Produced with B3 (3 mm x 6.5 mm orifice)	
		% Retained	% Cumulative Passing	% Retained	% Cumulative Passing
100	150	9.9	90.1	8.2	91.8
120	125	5.7	84.4	3.5	88.3
140	106	6.7	77.7	5.1	83.2
170	90	6.2	71.5	5.7	77.5
200	75	8.3	63.2	10.7	66.8
230	63	12.5	50.7	10.5	56.3
270	53	15.2	35.5	15.7	40.6
325	45	15.2	20.3	16.7	23.9
400	38	8.7	11.6	10.5	13.4
450	32	6.8	4.8	8.2	5.2
500	25	4.1	0.7	3.9	1.3
pan	0	0.7	-	1.3	-

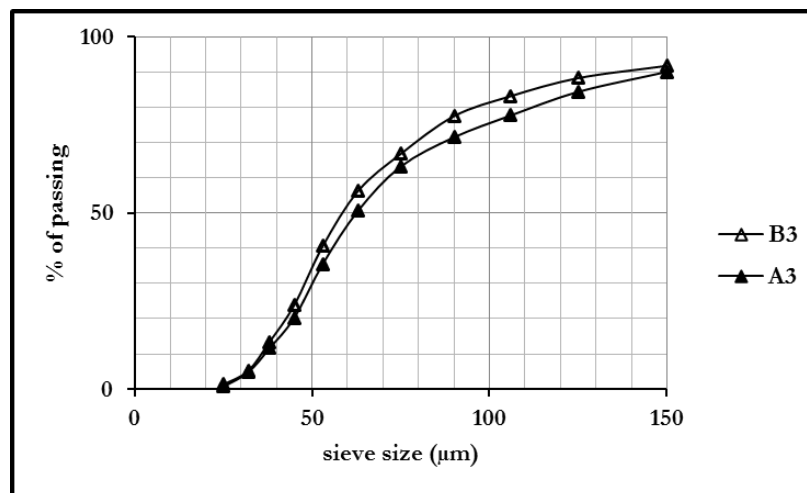


Fig. 9. Cumulative percentage of undersize of copper powder produced with metal flow rate ~ 26 kg/min.

Table 6. Comparison of the yield of the production with each orifice.

Size ( $\mu\text{m}$ )	Cumulative percentage of passing (% yield of undersize)					
	orifice 13 kg/min		orifice 16 kg/min		orifice 26 kg/min	
	A1	B1	A2	B2	A3	B3
	$\varnothing 5$ mm	3 mm x 6.5 mm	$\varnothing 6$ mm	3 mm x 9.5 mm	$\varnothing 7$ mm	3 mm x 12 mm
150	93.2	95.3	91.4	93.1	90.1	91.8
125	92.3	94.2	88.0	91.2	84.4	88.3
106	88.7	91.6	82.1	87.6	77.7	83.2
90	84.6	86.4	75.3	82.4	71.5	77.5
75	75.3	79.6	67.8	73.1	63.2	66.8
63	66.9	70.4	58.3	63.5	50.7	56.3
53	53.8	58.6	42.6	49.6	35.5	40.6
45	41.2	45.2	25.7	34.3	20.3	23.9
38	24.5	29.1	16.3	20.2	11.6	13.4
32	11.2	13.8	7.6	9.4	4.8	5.2
25	4.2	5.3	2.8	3.2	0.7	1.3
0	-	-	-	-	-	-

The most widely used indicator to describe particle size distribution are D-values. The D10, D50 and D90 are commonly used to represent the midpoint and range of the particle size [18, 19]. Particle size distribution have been traditional calculated based on sieve analysis results, creating S-curve of cumulative percentage against sieve size, and find the intercepts for 10%, 50% and 90% mass. They give an indication of the fine (D10), coarse (D90) and median (D50) particle size. The most common values used for measuring the distribution width is the range which calculated by equations below [20]:

$$\text{Particle Size Distribution Range} = D90 - D10 \quad (4)$$

The D-values measure form the S-curves are shown in Table 7 and Fig. 10.

Table 7. The D-values and the Ranges of distribution.

Metal flow rate	Produced with	D10 ( $\mu\text{m}$ )	D50 ( $\mu\text{m}$ )	D90 ( $\mu\text{m}$ )	Range (D90-D10)
13 kg/min	A1 ( $\varnothing 5$ mm)	32	51	112	80
	B1 (3 mm x 6.5 mm)	29	48	100	71
19 kg/min	A2 ( $\varnothing 6$ mm)	34	58	140	106
	B2 (3 mm x 9.5 mm)	32	54	120	88
26 kg/min	A3 ( $\varnothing 7$ mm)	38	62	150	112
	B3 (3 mm x 12 mm)	36	58	135	99



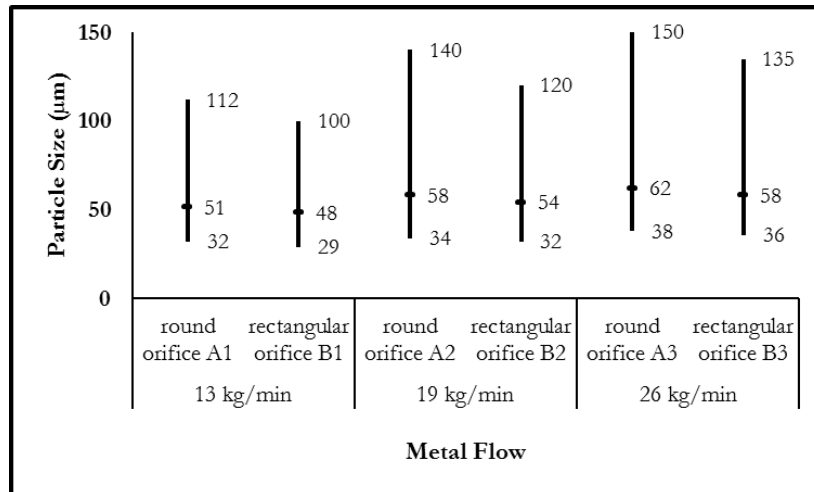


Fig. 10. Particle size distribution range from D10 to D90 with D50.

The results show that at the same metal flow rate, production with wide-thin metal stream from rectangular orifices provided narrower range of particle size distribution and smaller D50 than production with round orifices. It might explain that metal stream from rectangular orifices has wider flat area which face directly to the water jets and thinner stream which made easier to be atomized. While the outer curve of round section metal stream will not impinge perpendicular to water jets and more thickness in the middle make it be less atomized (see Fig. 11).

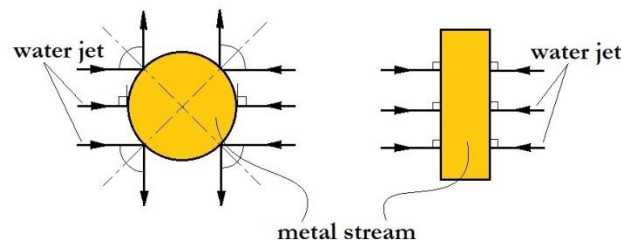


Fig. 11. Impinging of water jet and metal stream comparison between round and rectangular cross section metal stream.

From the yields, D50 and ranges of distribution which shown in Table 6, 7 and Fig. 10, it could be said that production with the thin flat metal stream can produce more yield of finer resolution powder at the same production rate. And because of narrower range of size distribution we can obtain more yield of any specific particle size.. On the other hand, while compare the results of A1 (13 kg/min) with B2 (19 kg/min) or A2 (19 kg/min) with B3 (26 kg/min) their D-values and range are very similar. It could be said that the production of flat metal stream can produce as similar resolution as the production of round section stream but higher production rate.

#### 4. Conclusions

The results indicated that the shape of molten metal stream can affect the resolution of atomized metal powder significantly. At the equally molten metal's flow rates, the production with the flat metal stream from rectangular section orifices can make smaller size of D10, D50 and D90, narrower range of size distribution than the production using round section orifices.

The assumption for describing the result is the metal stream which flows from rectangular orifice is wider and thinner, has larger flat surface area faced to the water jets which made more chance to be collided directly by water jets and split into smaller particle. While the metal stream which flows from round orifice is thicker stream which is more difficult to collide to the center of the stream.

For the same shape of molten metal orifice, producing with the smaller size of orifice or lower metal flow rate made D10, D50 and D90 tend to become smaller. That means increasing of the ratio of water/metal flow rate will made higher yield of finer particle.

At the same process conditions, using rectangular cross section orifice made higher yield of finer resolution powder than producing with the circular cross section orifice. That means the process consumed the same amount of energy but produced finer powder.

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