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## Analysis of Multi-objective Optimal Dispatch of Cogeneration with Thermal Energy Storage for Building Energy Management System

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**Abstract.** This paper presents analysis of the multi-objective optimal operation of designed BEMS which contains cogeneration or combined heat and power (CHP) and thermal energy storage (TES) as energy sources. The previously designed BEMS consists of CHP as the main energy supply with absorption chiller and auxiliary boiler. It is observed that there is excessive heat energy from CHP operation which is enough for further utilization. In this paper, TES is additional component to utilize excessive heat energy released from CHP operation. TES cooperates with CHP and auxiliary boiler to supply heat energy to meet the cooling load demand in the building. There are two objective functions for consideration, namely, total operating cost (TOC) and total carbon dioxide emission (TCOE). The multi-objective framework combines both objective functions and employs the weighted sum of TOC and TCOE. Furthermore, we vary initial state of TES from 0-20% of TES's capacity and analyze its effect on TOC and TCOE. We apply the multi-objective approach to a large shopping mall. Numerical results show that setting initial state of TES to 0% can offer more reduction of TOC and TCOE than other initial conditions. The multi-objective optimal operation converges to minimum TOC when a weighting factor is 0. On the other hand, it converges to the minimum TCOE when the weighting factor is 1. In addition, the trade-off curve showing a relationship between TOC and TCOE provides operating points which depends on operator's decision criterion.

**Keywords:** Combined heat and power (CHP), thermal energy storage (TES), building energy management system (BEMS), multi-objective approach, energy efficiency.

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## 1. Introduction

Building energy management system (BEMS) has become popular research topic for many years due to limitation of energy source and rising trends of energy consumption. Besides, the main electricity usage in the building generally comes from power grids which provide high price of electricity charge depending on on/off peak hour and also generates high carbon dioxide (CO<sub>2</sub>) emission to atmosphere. Generally, conventional buildings such as offices, commercial buildings, shopping malls, hotels, or homes contain mainly three types of load, i.e., electrical, cooling, and heating loads. Both public and private sectors always seek solution for energy efficiency usage management such as seeking other energy sources, implementing network management, design of smart grid [1-5]. One of the promising technologies usually applies with BEMS is Cogeneration or combined heat and power (CHP).

CHP is simultaneous production of heat and power [6-7]. CHP employs only a single source to obtain two types of output which heat energy is from fuel combustion in process. Besides, CHP is promoted as an energy source in Thailand Power Development plan (PDP2015) [8] since it offers more efficiency than conventional generation. Therefore, many researches focus on how to apply CHP to BEMS. Not only CHP system but solar and conventional energy sources are often implemented to supply to energy demand in commercial building. The goal is to minimize the life-cycle cost and profits from exporting onsite-generated electrical energy to grids [9]. Economic operation of CHP is designed under emission constraints in order to minimize the cost and pollutant emission from CHP system [10]. There is model development to achieve optimal dispatch of electrical, cooling, and heating supply to load in a small industry. In particular, economic operation aims to reduce investment cost and time, and gain more benefits and comfort [11]. Subsequently, the CHP model is modified to suit application of a large shopping mall [12]. The modified model consists of CHP cooperating with boiler and chiller to respond the electrical and cooling loads in the shopping mall. It is observed that there is some excessive heat energy releases from CHP to the atmosphere. The amount of excessive heat is enough for further utilization. Therefore, thermal energy storage (TES) is installed to utilize excessive heat energy from CHP operation and dispatch strategy is designed by taking into account of TES constraints [13]. The installed TES cooperates with CHP and the boiler to supply enough heat energy to meet the demand in the building. Objective functions are to minimize total operating cost (TOC) and total CO<sub>2</sub> emission (TCOE) of BEMS. As a result, CHP with TES can offer reduction of TOC and TCOE since TES can reduce operation of the boiler. However, relationship of two objective functions has not been investigated.

In this paper, we propose a multi-objective optimal operation of CHP with TES in order to find the relationship between economic and environmental optimal operations. Furthermore, we will analyze the effect of the multi-objective operation when initial state of TES is varied. Optimal operation is described in terms of trade-off relationship between TOC and TCOE. The results will enable the operator to select the preferred operating point.

This paper is organized as follows. Section 2 is system description of the proposed CHP with TES. Section 3 presents objective functions and mathematic model of TES. The energy dispatch strategies of both electrical and cooling energy are presented in section 4. System parameters and load profile of test system is in Section 5. Section 6 illustrates the trade-off results. Conclusions are given in section 7.

## 2. Cogeneration with Thermal Energy Storage for Building Energy Management System

Generally, conventional buildings employ electrical energy from power grids in order to response load demands in the buildings. Power grids require high electricity charges, especially on-peak hours and most of supply-side power plants still use fossil fuel which cause large amount of CO<sub>2</sub> emission to the atmosphere. Therefore, the goal of designed cogeneration system is to reduce operating cost and CO<sub>2</sub> emission. The cogeneration or CHP becomes part of the system as an efficient energy source. As excessive thermal energy is found from CHP operation in previous research [12], thermal energy storage is installed to utilize the excessive thermal energy [13]. Accordingly, the proposed BEMS consists of a CHP system, an auxiliary boiler, an absorption chiller, and a thermal energy storage (TES) an energy supplies of BEMS.

The conventional buildings normally contain two types of loads, electrical and cooling loads. Energy supply from the proposed BEMS will be utilized to meet load demands in the buildings. Load demands of BEMS are taken from load profiles of a large shopping mall. Diagram of CHP and TES in response to load demands of building is shown as Fig. 1.

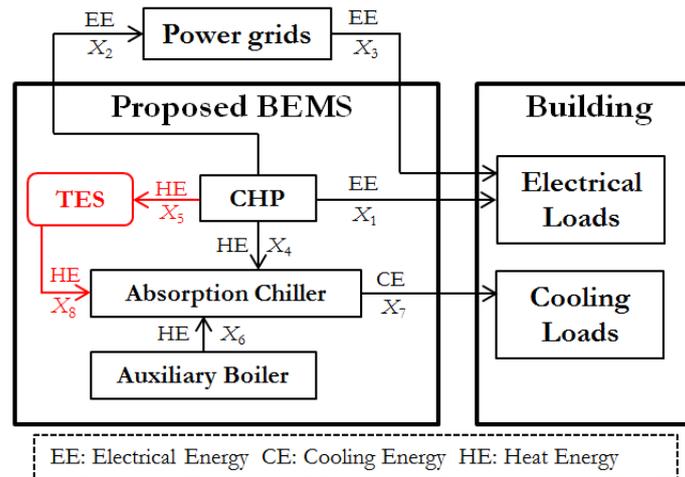


Fig. 1. Diagram of CHP and TES in response to load demands of building.

CHP mainly supplies energy to meet energy load demands in the building due to the production of simultaneous electrical and heat energy. In this study, BEMS is connected to power grids for power trading. Imported electrical energy from power grids is needed when CHP cannot adequately supply to demand loads. BEMS can earn revenues from exporting excessive electrical energy to power grids. Since heat energy is produced by CHP, the absorption chiller is equipment which converts heat energy to cooling energy then supplies to the cooling load in the building. Moreover, the auxiliary boiler plays a role of supplying heat energy in case that CHP cannot fulfill the demand load. In some cases, CHP generates heat energy but there is no cooling load. This heat energy will be stored in TES. When CHP and auxiliary boiler cannot supply enough heat energy to meet the demand, TES will cooperate to supply heat energy to absorption chiller.

### 3. Problem Formulation

The goal of cogeneration system is to achieve reductions of energy operating cost and CO<sub>2</sub> emission by applying TES. Optimal dispatch strategy is formulated by applying two objective functions. Concerning issues of energy cost and CO<sub>2</sub> emission, economic and environmental optimal operations are separately considered and subject to operating constraints of CHP and other equipment including TES. All physical components are modeled as linear function and neglecting internal losses.

#### 3.1. Economic Optimal Operation

The economic optimal operation is objective function which aims to minimize total operating cost, TOC (baht). TOC is a result from the sum of energy cost (EC) and demand charge cost (DCC). EC is the sum of energy operating cost from components which can be calculated from energy cost of CHP, income and expense from power trading with power grids, and energy cost of the auxiliary boiler. DCC is calculated from maximum imported power from power grids of the whole interested periods. The economic optimal operation can be represented as follows.

$$TOC = EC + DCC \quad (1)$$

$$EC = \sum_{k=1}^{nd} (C_{CHP} (x_{1,k} + x_{2,k}) - q_k x_{2,k} + p_k x_{3,k} + c_{AB} x_{6,k}) \quad (2)$$

$$DCC = \frac{d_{PG}}{\Delta t} \max_{h=1, \dots, nd} x_{3,k} \quad (3)$$

where  $x_{i,k}$  is energy flow (MWh) following Fig. 1 in time interval of  $k$ .  $c_{CHP}$  and  $c_{AB}$  are operating cost of the CHP and the auxiliary boiler operation which depend on fuel piece,  $q_k$  is electrical energy base price,  $p_k$

is electrical energy charge price during on-peak and off-peak hour,  $d_{PG}$  is demand charge depending on maximum imported power from power grids,  $n$  is the number of time interval in one day,  $d$  is the number of days, and  $\Delta t$  is time duration of each time interval.

### 3.2. Environmental Optimal Operation

Effective BEMS concerns not only the operation cost, but also greenhouse gas emission. The environmental optimal operation aims to minimize CO<sub>2</sub> emission which is defined in terms of total carbon dioxide emission, TCOE (tonCO<sub>2</sub>). TCOE is calculated from the sum of CO<sub>2</sub> emission of electrical energy production process of CHP, imported power from power grids, and heat energy production process of the auxiliary boiler. The environmental optimal operation can be represented as follows.

$$TCOE = \sum_{k=1}^{nd} (EF_{CHP,CO_2}(x_{1,k} + x_{2,k}) + GEF(x_{3,k}) + \frac{EF_{AB,CO_2}(x_{6,k})}{\eta_{AB}}) \quad (4)$$

where  $EF_{CHP,CO_2}$  and  $EF_{AB,CO_2}$  are CO<sub>2</sub> emission factors of CHP and auxiliary boiler operations. These factors depend on fuel price. GEF is grid emission factor and  $\eta_{AB}$  is boiler's efficiency.

### 3.3. Multi-objective Optimal Operation

Since two objective functions are important, we can combine both economic and environmental optimal operations by employing a weighting factor ( $\alpha$ ) and normalization of objective functions. A multi-objective function denoted by  $J$  is defined as follows.

$$J = (1 - \alpha) \frac{TOC}{TOC_{min}} + \alpha \frac{TCOE}{TCOE_{min}} \quad (5)$$

The weighting factor is constant real number and varies from 0 to 1. Minimizing (5) will result in a multi-objective optimal operation.  $TOC_{min}$  is the minimum of TOC, and  $TCOE_{min}$  is the minimum of TCOE.

### 3.4. Thermal Energy Storage Model

TES is equipment used to store excessive heat from CHP and supply heat energy to the building load. The mathematic model is based on Hashemi's paper [11]. Heat charge and discharge shall not exceed ( $R_1$ ) and discharge ( $R_2$ ) rates. Besides, state of charge of TES can be calculated from the difference of heat charge to TES and heat discharge from TES. Constraints of TES can be described as follows:

$$\epsilon(x_{5,k}) \leq R_1 \quad (6)$$

$$\frac{1}{\delta}(x_{8,k}) \leq R_2 \quad (7)$$

$$x_{9,k} = \text{init}(1 - \mu)^k + \sum_{j=1}^k (\epsilon(x_{5,j}) - \frac{1}{\delta}(x_{8,k})) (1 - \mu)^{k-j+1} \quad (8)$$

$$S_{min} \leq x_{9,k} \leq S_{max} \quad (9)$$

where  $\epsilon$  and  $\delta$  are TES charge and discharge efficiency,  $R_1$  and  $R_2$  are charge and discharge rates. The variable  $x_{9,k}$  is state of charge at time  $k$ . Loss coefficient of TES is represented by  $\mu$ .  $\text{init}$  is initial heat energy stored in TES.  $S_{min}$  and  $S_{max}$  are minimum and maximum states of TES.

## 4. Energy Dispatch Strategies

Although there are two separate objective functions, BEMS operates under the same constraints. Dispatch strategies or constraints are characterized by types of building's load. Dispatch strategies in this section are

classified into two types, electrical energy (EE) dispatch and cooling energy (CE) dispatch. Optimization problem is formulated as a linear program (LP) which can be efficiently solved by LP solvers.

EE dispatch is a function of electrical load ( $U_k$ ) in the building. Energy supplies compose of CHP and power grids. EE dispatch contains two conditions. Firstly, CHP will shut down when there is no  $U_k$ . On the other hand, CHP and power grids supply EE to the load under limitations of minimum and maximum production of CHP ( $P_{CHP,min}$  and  $P_{CHP,max}$ ). EE and HE production of CHP will be operated at power-to-heat ratio (P2H). Ramp rate of CHP is considered by the difference of EE generation in pervious and current states. The EE dispatch can be written as follows.

if  $U_k = 0$ , then

$$x_{1,k} = x_{2,k} = x_{4,k} = x_{5,k} = 0$$

else

$$P_{CHP,min}\Delta t \leq x_{1,k} + x_{2,k} \leq P_{CHP,max}\Delta t$$

$$\frac{x_{1,k} + x_{2,k}}{x_{4,k} + x_{5,k}} = P2H$$

$$\left| (x_{1,k} + x_{2,k}) - (x_{1,k-1} + x_{2,k-1}) \right| \leq R_{CHP} \Delta t$$

end

$$x_{1,k} + x_{3,k} = U_k$$

For the CE dispatch, heat energy sources consist of CHP, the auxiliary boiler, and TES. All these components supply heat energy to the absorption chiller in order to convert into cooling energy for cooling load ( $C_k$ ). The CE dispatch provides four conditions of heat/cooling energy management. Firstly, there is no heat energy from any source to the chiller, but there is excessive heat charging to TES while CHP still runs the operation to meet electrical load. The excessive heat charging to TES is limited by charge rate ( $R_1$ ). Secondly, there is cooling load  $C_k$  less than minimum cooling production of chiller ( $CP_{AC,min}$ ). CHP and TES will supply HE to the chiller. The chiller operates at its minimum level to maintain temperature in the building. Therefore, there is no need to operate the boiler and there is no excessive heat charging to TES during discharging heat. Thirdly, when  $C_k$  is over minimum operation of the chiller and CHP supplies enough heat, boiler will not be enabled. CHP and TES cooperate to supply HE to the chiller and covert to CE at level of  $C_k$ . Finally, when CHP does supply enough HE to meet  $C_k$ , the auxiliary boiler has a role to supply enough heat to the chiller in conjunction of CHP and TES operation. The chiller operates at  $C_k$  and does not exceed the maximum cooling production of chiller ( $CP_{AC,max}$ ) and the heat production from CHP and the boiler. The CE dispatch can be summarized as follows.

if  $C_k = 0$ , then

$$x_{4,k} = x_{6,k} = x_{7,k} = x_{8,k} = 0$$

$$x_{9,k} = (x_{9,k-1} + x_{5,k})(1 - \mu)$$

$$\epsilon(x_{5,k}) \leq R_1 \Delta t$$

else if  $C_k \leq CP_{AC,min} \Delta t$ , then

$$(x_{4,k} + x_{8,k})COP_{AC} = x_{7,k}$$

$$\frac{1}{\delta} x_{8,k} \leq R_2 \Delta t$$

$$x_{9,k} = (x_{9,k-1} - x_{8,k})(1 - \mu)$$

$$x_{5,k} = x_{6,k} = 0$$

$$x_{7,k} = CP_{AC,min} \Delta t$$

elseif  $C_k \leq \frac{P_{CHP,max}\Delta t}{P2H} COP_{AC}$ , then

$$\begin{aligned}
 (x_{4,k} + x_{8,k})\text{COP}_{AC} &= x_{7,k} \\
 \frac{1}{\delta}(x_{8,k}) &\leq R_2\Delta t \\
 x_{9,k} &= (x_{9,k-1} - x_{8,k})(1 - \mu) \\
 x_{5,k} &= x_{6,k} = 0 \\
 x_{7,k} &= \min\left(C_k, \frac{P_{\text{CHP,max}}\Delta t}{P_{2H}}\text{COP}_{AC}\right)
 \end{aligned}$$

else

$$\begin{aligned}
 (x_{4,k} + x_{6,k} + x_{8,k})\text{COP}_{AC} &= x_{7,k} \\
 \frac{1}{\delta}(x_{8,k}) &\leq R_2\Delta t \\
 x_{9,k} &= (x_{9,k-1} - x_{8,k})(1 - \mu) \\
 \text{HP}_{AB,\min}\Delta t &\leq x_{6,k} \leq \text{HP}_{AB,\max}\Delta t \\
 x_{5,k} &= 0 \\
 x_{7,k} &= \min\left(C_k, \text{CP}_{AC,\max}\left(\frac{P_{\text{CHP,max}}\Delta t}{P_{2H}} + \text{HP}_{AB,\max}\Delta t\right)\text{COP}_{AC}\right)
 \end{aligned}$$

end.

The multi-objective optimal operation is formulated as a linear program (LP) which can be efficiently solved by LP solvers.

## 5. System Parameters

In case study, we consider load profiles of a large shopping mall in Bangkok, Thailand as a test system. Normally, the shopping mall utilizes the electricity from Metropolitan Electricity Authority (MEA) with 69-kV distribution grid. Figure 2 shows electrical load profile for 7 days ranging from 5 MW to 24 MW. Figure 3 shows calculated cooling load profile for 7 days ranging from 0 MW to 43 MW. Therefore, parameters of major components of BEMS are based on the test system of BEMS [12, 13].

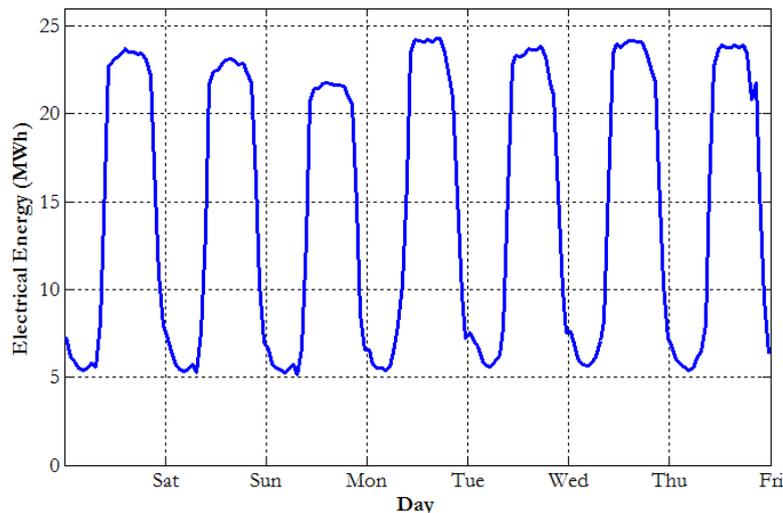


Fig. 2. Electrical load profile of large shopping mall for 7 days.

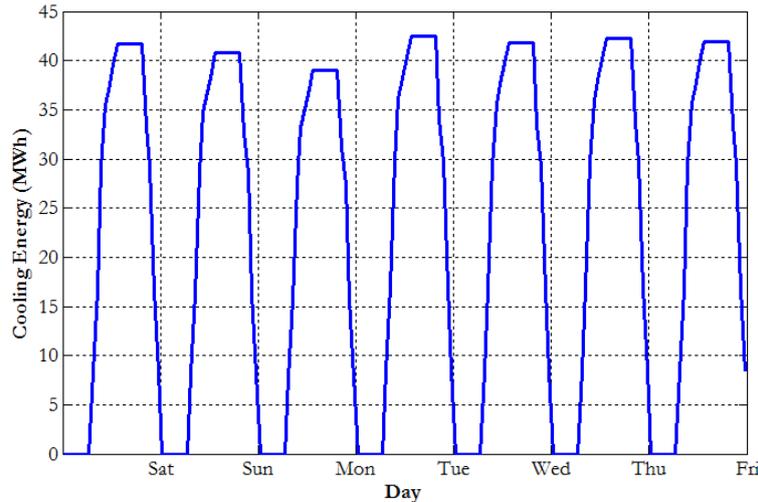


Fig. 3. Calculated cooling load profile of large shopping mall for 7 days.

For CHP system, BEMS utilizes gas turbine as CHP system due to appropriate size and capacity with the demand. Gas turbine runs with high temperature steam which provides benefits to the cooling load of the building [7]. There is a research of TOC and TCOE by varying CHP size from 22 MW to 25 MW [12]. In our test system, electrical load profile has peak demand of 24 MW. Thus, we choose 24 MW of CHP. For the absorption chiller, double-effect absorption chiller 12,000-TR is selected which matches energy output of CHP system. Coefficient of Performance (COP) of chiller is 1.1 following regulation on energy usage for building recommendation [12]. For auxiliary boiler, industrial boiler using natural gas is chosen with capacity of 45 MMBtu/hr. Moreover, the boiler with natural gas can obtain 75% of thermal efficiency at full load [12, 14] and CO<sub>2</sub> emission factor from natural gas combustion ( $EF_{AB,CO_2}$ ) is 0.1810 tCO<sub>2</sub> [15].

Natural gas price (baht/MMBtu) can be calculated following National Energy Policy Commission [16] as follows.

$$NGP = APNG + \min(0.0933 \times APNG, 11.4759) + 12.0654 \quad (10)$$

where APNG is monthly average of natural gas price (baht/MMBtu) which data can be found from the Department of Mineral Fuels, Ministry of Energy [17]. The second term is payment of natural gas supply and distribution depends on types of customer [16]. The last term is price of gas transportation [18].

In Thailand, there are two types of electricity price, i.e., time-of-day (TOD) and time-of-use (TOU). TOU rate is adopted in this study. TOU tariff composes of energy charge, demand charge, service charge, power factor charge, fuel adjustment (Ft), and VAT. However, only energy charge and demand charge are considered in this study and the rest are neglected. BEMS pays 4.1283 and 2.6107 baht/kWh for energy charge on-peak and off-peak time, respectively. The demand charge price for large general service with 69-kV is 74.14 baht/kW [19]. The selling price from CHP to power grid can refer from the wholesale prices that EGAT sells electricity to MEA [22]. Furthermore, electricity price from CHP is referred in [20]. For grid emission factor (GEF) of Thailand, CO<sub>2</sub> emission is estimated when BEMS uses electricity from power grids [21]. All parameter are summarized in Table 1.

## 6. Numerical Results and Discussions

The multi-objective optimal operation of this work is presented as trade-off relationship between economic and environmental optimal operations. Besides, initial state of TES is varied along with weighting factor of multi-objective operation to observe TOC and TCOE trends.

Table 1. System parameters.

Description	Notation	Value
<b>CHP system</b>		
Rated power (MW)	-	24
Electrical energy efficiency (%)	$\eta_{\text{CHP,EE}}$	33.90
Power-to-heat ratio	P2H	0.9244
Maximum power production (MW)	$P_{\text{CHP,max}}$	24
Minimum power production (MW)	$P_{\text{CHP,min}}$	4.8
Electrical energy ramp rate (MW)	$R_{\text{CHP}}$	24
CO <sub>2</sub> emission factor (tCO <sub>2</sub> /MWh)	$EF_{\text{CHP,CO}_2}$	0.5349
<b>Auxiliary boiler</b>		
Rated heat power (MW)	-	13.1882
Efficiency (%)	$\eta_{\text{AB}}$	75
Maximum heat production (MW)	$HP_{\text{AB,max}}$	13.1882
Minimum heat production (MW)	$HP_{\text{AB,min}}$	2.6376
CO <sub>2</sub> emission factor from natural gas combustion (tCO <sub>2</sub> /MWh)	$EF_{\text{AB,CO}_2}$	0.1810
<b>Absorption chiller</b>		
Rated cooling power	-	42.2
Coefficient of performance	$\text{COP}_{\text{AC}}$	1.1
Maximum cooling production (MW)	$\text{CP}_{\text{AC,max}}$	42.2
Minimum cooling production (MW)	$\text{CP}_{\text{AC,min}}$	8.44
<b>Thermal energy storage</b>		
Rated heat power (MW)	-	50
Heat charge rate (MW)	$R_1$	15
Heat discharge rate (MW)	$R_2$	15
Charging efficiency	$\epsilon$	0.95
Discharging efficiency	$\delta$	0.95
TES loss coefficient	$\mu$	0.001
Initial heat energy in TES (MW)	init	0-10
Maximum heat storage (MW)	$S_{\text{max}}$	50
Minimum heat storage (MW)	$S_{\text{min}}$	5
<b>Others</b>		
Electrical energy load in time interval k (MWh)	$U_k$	-
Cooling energy load in time interval k (MWh)	$C_k$	-
Electrical energy base price during on-peak, off-peak (baht/kWh)	$q_k$	3.2504, 2.0198
Electrical energy charge during on-peak, off-peak (baht/kWh)	$p_k$	4.1283, 2.6107
Demand charge (baht/kW)	$dp_G$	74.14
Grid Emission Factor (ton/Mwh)	GEF	0.5994
Time duration of each interval (hour)	$\Delta t$	1
Number of time interval per day	$n$	24
Number of days in week	$d$	7
Average Price of Natural Gas (baht/MMBtu)	APNG	179.87

### 6.1. Effect with TOC and TCOE from Initial State of Thermal Energy Storage

In this subsection, we analyze improvement on energy efficiency by varying the initial state of TES and observing TOC and TCOE of both economic and environmental optimal operations. Initial states of TES are set at 0%, 10%, and 20% of TES capacity which is 50 MW. In addition, we vary the weighting factor  $\alpha$  of multi-objective optimal operation and compare the results to the case of BEMS without TES. Table 2 summarizes the results. It is observed that for any choice of weighting factor, increasing initial state of TES

causes TOC and TCOE increase. For instance, when  $\alpha$  is chosen as 0.25, TOC for 0% initial state is 5,942,529 baht, TOC for 10% initial state is 5,982,898 baht, and TOC for 20% initial state is 6,049,307 baht. For BEMS without TES, TOC is 7,258,155 baht. Thus, BEMS with TES can reduce TOC from 16.7% to 18.1% compared to that of BEMS without TES. We observe a similar trend for environmental operation, namely, TCOE for 0% initial state is 1,576 tCO<sub>2</sub>, TCOE for 10% initial state is 1,585 tCO<sub>2</sub>, and TCOE for 20% initial state is 1,595 tCO<sub>2</sub>. For BEMS without TES, TCOE is 1,664 tCO<sub>2</sub>. Therefore, BEMS with TES can reduce TCOE from 4.1% to 5.3% compared to that of BEMS without TES.

Based on results, it is observed that a lower initial state of TES offers much more reduction of TOC and TCOE for all choices of weighting factor ( $\alpha$ ). CHP normally generates electrical and heat energy based on P2H ratio. Importing electrical energy from power grids is an expensive option due to large impact on TOC and TCOE. Therefore, CHP has to produce electrical energy to supply electrical load for the first priority. Moreover, BEMS enables CHP not only to produce electrical energy for EE demand, but also coordinate with TES to manage excessive heat from CHP. In case of large initial state of TES, the remaining space for heat storage is small. If electrical energy generated by CHP is not sufficient to meet the EE demand, BEMS has to import electrical energy from power grids which will effect to TOC and TCOE.

The results in Table 2 confirm that for any choice of initial state of TES, increasing weighting factor  $\alpha$  causes TOC increase but TCOE decrease. BEMS with TES yields significant improvement compared to that of BEMS without TES.

## 6.2. Relationship between TOC and TCOE

In this subsection, we analyze the relationship between economic optimal operation and environment optimal operation when we apply the multi-objective optimal dispatch strategy to BEMS. The multi-objective function of Eq. (5) is minimized and we vary weighting factor  $\alpha$  from 0 to 1 and initial state of TES from 0-20%. In numerical simulation, we select 2500 samples of  $\alpha$  and determine the optimal objective function. Figure 4 shows the results of multi-objective optimal operation as function of weighting factor  $\alpha$  and initial state of TES. It is observed that the multi-objective operation converges to economic optimal operation which yields minimum TOC when  $\alpha = 0$ . On the other hand, the multi-objective operation converges to the environmental optimal operation which gives minimum TCOE when  $\alpha = 1$ . Table 2 shows TOC and TCOE of the multi-objective operation by varying  $\alpha$  and initial state of TES. It is noted that for a given initial state of TES, some values of  $\alpha$  yield the same optimal TOC and TCOE.

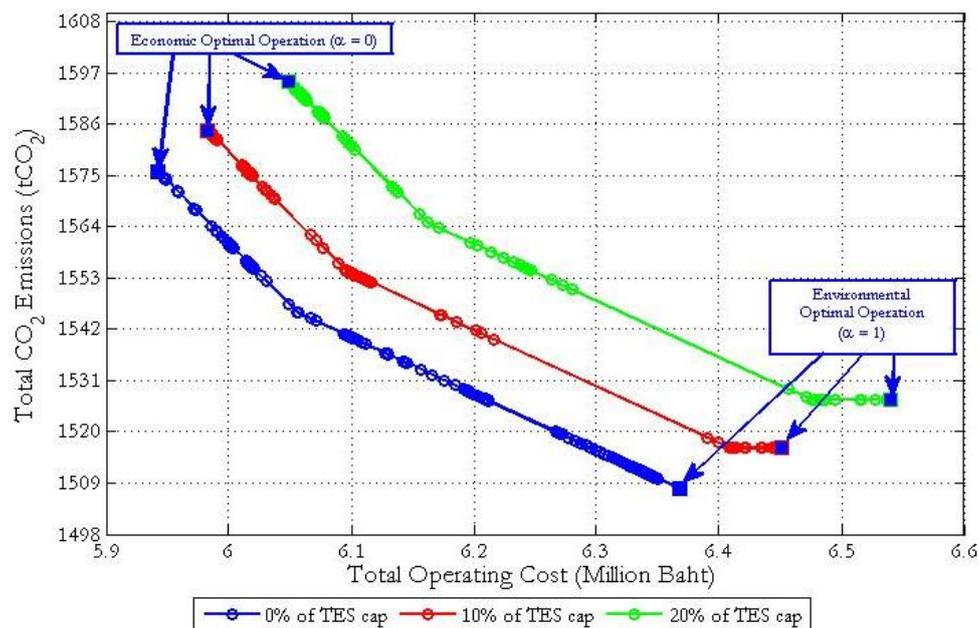


Fig. 4. Trade-off relationship between economic and environmental optimal operation.

Table 2. TOC and TCOE by varying  $\alpha$  and initial state of TES.

$\alpha$	Optimal Operation*	Initial state of TES			BEMS without TES
		0%	10%	20%	
0	TOC	5,942,529	5,982,898	6,049,307	7,246,962
	TCOE	1,576	1,585	1,595	1,672
0.1	TOC	5,942,529	5,982,898	6,049,307	7,246,962
	TCOE	1,576	1,585	1,595	1,672
0.2	TOC	5,942,529	5,982,898	6,049,307	7,246,962
	TCOE	1,576	1,585	1,595	1,672
0.3	TOC	5,942,529	5,982,898	6,049,307	7,258,155
	TCOE	1,576	1,585	1,595	1,664
0.4	TOC	5,942,529	5,982,898	6,049,307	7,258,155
	TCOE	1,576	1,585	1,595	1,664
0.5	TOC	6,055,988	6,096,416	6,162,882	7,305,612
	TCOE	1,546	1,554	1,565	1,649
0.6	TOC	6,055,988	6,096,416	6,162,882	7,305,612
	TCOE	1,546	1,554	1,565	1,649
0.7	TOC	6,368,305	6,408,781	6,475,291	7,543,828
	TCOE	1,508	1,517	1,527	1,618
0.8	TOC	6,368,305	6,408,781	6,475,291	7,543,828
	TCOE	1,508	1,517	1,527	1,618
0.9	TOC	6,368,305	6,408,781	6,475,291	7,543,828
	TCOE	1,508	1,517	1,527	1,618
1	TOC	6,368,305	6,451,254	6,539,845	7,543,828
	TCOE	1,508	1,517	1,527	1,618

\*Unit of TOC is baht and unit of TCOE is tCO<sub>2</sub>.

Figure 4 clearly displays trade-off relationship between TOC and TCOE and it depends on  $\alpha$  and initial state of TES. The trade-off curve has twofold benefits. First, it is useful for operator to choose optimal operating points. For example, if we choose 10% of the initial state of TES (red line), TOC is specified to be less than 6.09 Million baht, then TCOE should range from 1,554 tonCO<sub>2</sub> to 1,584 tonCO<sub>2</sub>. Second, it provides the limit of performance of optimal operations. In particular, TOC will not be less than 5.94 Million baht, and TCOE will not be less than 1,508 tCO<sub>2</sub>.

### 6.3. Energy Flow Analysis of Multi-Objective Optimal Operation

This subsection shows energy flow analysis of multi-objective optimal operation of BEMS with TES. We demonstrate energy flow for the case  $\alpha = 0.5$  and initial state of TES equal to 0%. As a result, BEMS with multi-objective operation offers TOC equals to 6,055,988 baht and TCOE equals to 1,546 tonCO<sub>2</sub> for load profiles in a whole week. Moreover, BEMS with TES can reduce TOC up to 17.1% and TCOE up to 6.2% when compared to that of BEMS without TES.

For a chosen operating point, we demonstrate optimal energy flow in one day. BEMS with TES normally operates to meet load demands in the building. Therefore, electrical energy from CHP production is mainly supplied to the electrical load. Moreover, BEMS will earn profits from exporting of excessive electrical energy during on-peak hour as in Fig. 5. The main heat energy from CHP production is supplied to the chiller. During off-peak hours, excessive heat energy is charged to TES at 00.00 to 07.00 as shown in Fig. 6. The optimal energy flow to electrical load is referred in Fig. 7. CHP system is the main component which supplies most of generated electrical energy to electrical load. It is observed that there is imported electrical energy from power grid during 07.00-09.00 because price of electrical energy importing at that time offers advantage to the operating cost over running operation of CHP. Figure 8 shows optimal cooling energy flow to cooling load. During on-peak hours, CHP system is still the main component which supplies heat energy to the cooling load indirectly. Moreover, heat energy from TES can reduce operation of the

boiler at on-peak hours which directly reduce TOC and TCOE compared to that of BEMS without TES. Figure 8 shows state of charge of TES, heat energy is charged to TES at 00.00-07.00. Afterwards during 7.00-17.00 and 22.00-24.00, heat energy is discharged from TES to supply heat together with CHP and the boiler. TES normally operates to charge and discharge to meet the cooling load demand in one day.

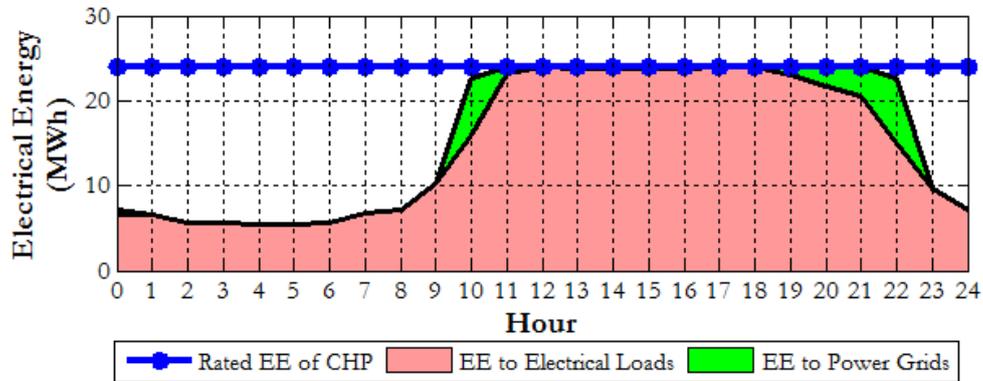


Fig. 5. Electrical energy production of CHP.

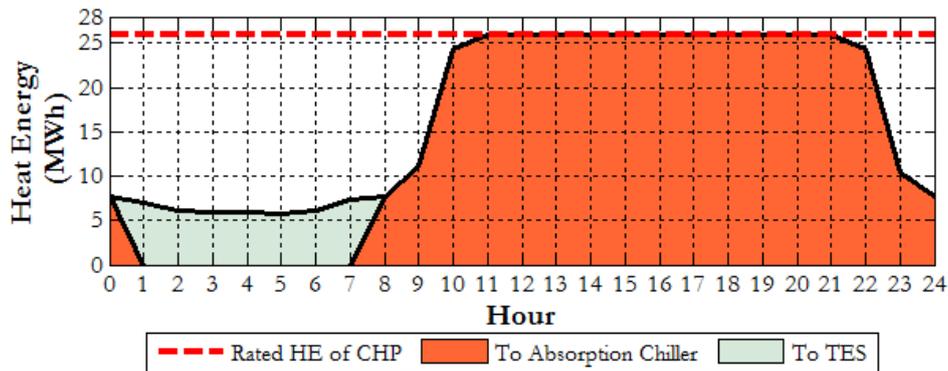


Fig. 6. Heat energy production of CHP.

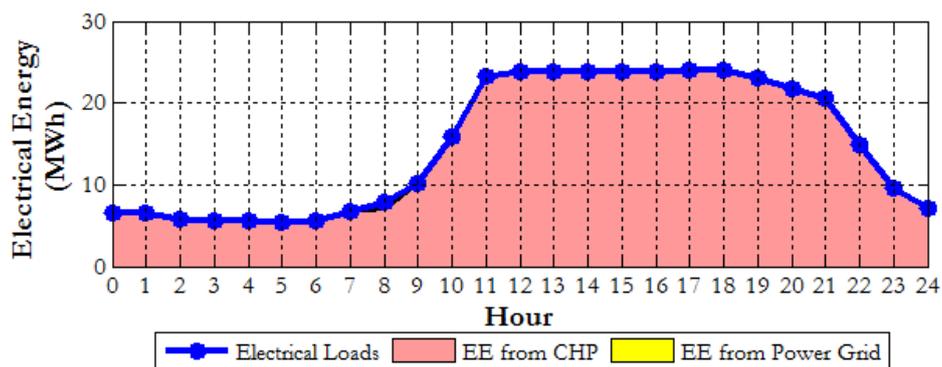


Fig. 7. Electrical energy flow to electrical load.

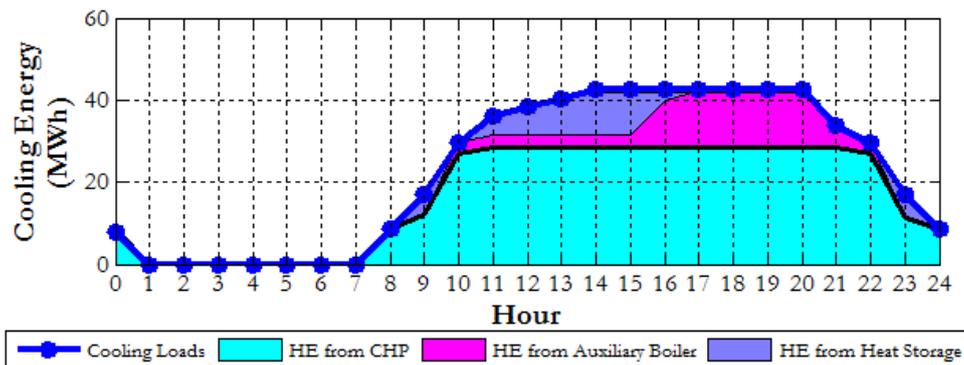


Fig. 8. Cooling energy flow to cooling load.

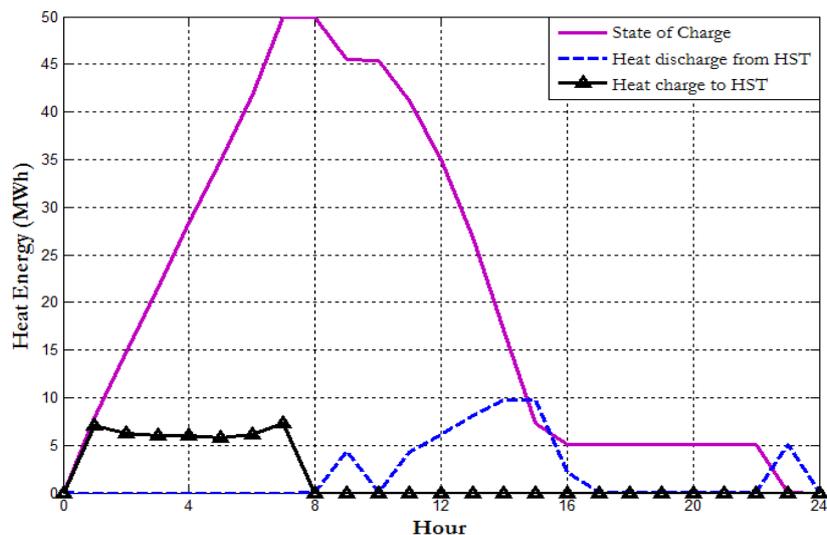


Fig. 9. State of charge of TES for multi-objective optimal operation.

## 7. Conclusions

In this paper, thermal energy storage (TES) is additional component in BEMS and coordinates with CHP for the main energy supply. TES stores excessive thermal energy which is generated by CHP under condition of no cooling load. TES plays a role as an energy source which supplies heat energy to absorption chiller when there is cooling load. Adding TES to BEMS, multi-objective optimal operation is applied to BEMS in order to analyze relationship between two distinct objective functions, TOC and TCOE. The relationship between TOC and TCOE represented as a trade-off curve offers many optimal solutions depending on operator's selection criterion. Moreover, varying initial state of TES gives a significant impact of TES on the multi-objective optimal operation. Lower level of initial state provides more reduction of TOC and TCOE.

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